

## Calorimetric Investigation of PrBr<sub>3</sub>-MBr Liquid Mixtures (M = Na, K, Rb, Cs)

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**ABSTRACT:** The molar enthalpies of mixing ( $\Delta_{\text{mix}}H_m$ ) in liquid alkali bromide-praseodymium(III) bromide mixtures have been measured with a Calvet-type high temperature microcalorimeter over the entire composition range at 1070 K. All of the melts are characterized by negative enthalpies of mixing with a minimum value shifted toward the alkali bromide-rich compositions that are located in the vicinity of  $x(\text{PrBr}_3) \sim 0.4$ . The magnitude of the mixing enthalpy depends on the ionic radius of the alkali metal, radius of the common halide ion, and the ionic radius of the lanthanide(III) cation.

### 1. INTRODUCTION

The present work is a continuation of our systematic research performed on PrBr<sub>3</sub>-based systems. Recently the phase diagrams of PrBr<sub>3</sub>-MBr (M = Li, Na, K, Rb, Cs) binary systems as well as thermodynamic functions of congruently melting M<sub>3</sub>PrBr<sub>6</sub> compounds were determined.<sup>1–5</sup> This work reports the results of mixing enthalpy measurements performed on PrBr<sub>3</sub>-MBr (M = Na, K, Rb, Cs) liquid systems over the whole composition range. All gathered experimental data were subsequently optimized by computer coupling of phase diagrams and thermochemistry (CALPHAD) method, as was done for analogous CeBr<sub>3</sub>-MBr binary systems.<sup>6</sup>

### 2. EXPERIMENTAL SECTION

**2.1. Chemicals.** Praseodymium(III) bromide was synthesized from the praseodymium oxide, Pr<sub>6</sub>O<sub>11</sub>, by a method analogous to that used for CeBr<sub>3</sub> synthesis.<sup>7</sup> The main steps of the synthesis involve: dissolution of praseodymium oxide in hot concentrated hydrobromic acid, crystallization of PrBr<sub>3</sub>·xH<sub>2</sub>O hydrates, their dehydration in the presence of ammonium bromide, melting of anhydrous praseodymium bromide, and its distillation under reduced pressure (~0.1 Pa) in a quartz ampule at 1150 K. PrBr<sub>3</sub> prepared in this way was of a high purity—min. 99.9 %. Chemical analysis was performed by mercurimetric (bromine) and complexometric (praseodymium) methods. The results were as follows: Pr, (36.96 ± 0.15) % (37.02 % theoretical); Br, (63.04 ± 0.11) % (62.98 % theoretical).

Sodium, potassium, rubidium, and cesium bromides were Merck Suprapur reagents (min. 99.9 %). Prior to use, they were progressively heated up to fusion under a gaseous HBr atmosphere. HBr in excess was then removed from the melt by argon bubbling.

All chemicals were handled in an argon glovebox with a measured fraction of water of about 2 mg·kg<sup>-1</sup> and continuous gas purification by forced recirculation through external molecular sieves.

**Table 1. Molar Enthalpies of Mixing  $\Delta_{\text{mix}}H_m$  and Interaction Parameters  $\lambda$  of the PrBr<sub>3</sub>–NaBr Liquid System at T = 1070 K**

$x(\text{PrBr}_3)$	$\Delta_{\text{mix}}H_m$		$\lambda$	
	$\text{kJ} \cdot \text{mol}^{-1}$	$\text{kJ} \cdot \text{mol}^{-1}$	$x(\text{PrBr}_3)$	$\text{kJ} \cdot \text{mol}^{-1}$
0.026	−0.825	−32.578	0.477	−5.054
0.044	−1.113	−26.459	0.528	−4.751
0.099	−2.543	−28.509	0.590	−4.522
0.152	−3.406	−26.424	0.649	−4.071
0.199	−4.214	−26.437	0.704	−3.421
0.249	−4.906	−26.235	0.750	−2.858
0.284	−5.017	−24.672	0.792	−2.476
0.324	−5.423	−24.759	0.823	−2.146
0.375	−5.435	−23.189	0.884	−1.537
0.430	−5.452	−22.243	0.923	−1.017

**2.2. Measurements.** The mixing experiments were all of the simple liquid–liquid type, performed under pure argon at atmospheric pressure. The Calvet-type high-temperature microcalorimeter, the mixing device, and the “break-off bubble” experimental method have all been described in detail elsewhere.<sup>7,8</sup> Calibration of the calorimeter was performed with  $\alpha\text{-Al}_2\text{O}_3$  (National Institute of Standards and Technology, NIST). A detailed description of the calorimeter constant determination, calibration of the thermocouple used to measure the experimental temperature, and discussion of errors that influence the results of the mixing enthalpy measurements was presented in our previous paper.<sup>7</sup> The relative error of mixing enthalpy determination was estimated as ± (6 to 8) %.

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**Table 2.** Molar Enthalpies of Mixing  $\Delta_{\text{mix}}H_m$  and Interaction Parameters  $\lambda$  of the  $\text{PrBr}_3$ – $\text{KBr}$  Liquid System at  $T = 1070$  K

$\Delta_{\text{mix}}H_m$		$\lambda$		$\Delta_{\text{mix}}H_m$		$\lambda$	
$x(\text{PrBr}_3)$	$\text{kJ}\cdot\text{mol}^{-1}$	$\text{kJ}\cdot\text{mol}^{-1}$	$x(\text{PrBr}_3)$	$\text{kJ}\cdot\text{mol}^{-1}$	$\text{kJ}\cdot\text{mol}^{-1}$	$x(\text{PrBr}_3)$	$\text{kJ}\cdot\text{mol}^{-1}$
0.052	−2.811	−56.611	0.542	−11.713	−47.194		
0.100	−5.957	−66.188	0.611	−10.645	−44.799		
0.155	−9.077	−69.413	0.659	−10.063	−44.805		
0.187	−10.128	−66.700	0.692	−9.174	−43.042		
0.240	−11.825	−64.793	0.744	−7.349	−38.584		
0.297	−12.830	−61.497	0.789	−5.452	−32.749		
0.343	−13.004	−57.697	0.843	−4.124	−31.159		
0.399	−13.312	−55.513	0.898	−2.925	−31.933		
0.454	−12.704	−51.249	0.947	−1.725	−34.368		
0.490	−13.278	−53.131					

**Table 3.** Molar Enthalpies of Mixing  $\Delta_{\text{mix}}H_m$  and Interaction Parameters  $\lambda$  of the  $\text{PrBr}_3$ – $\text{RbBr}$  Liquid System at  $T = 1070$  K

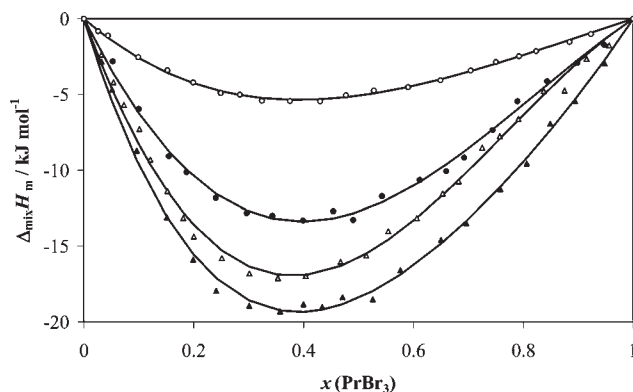
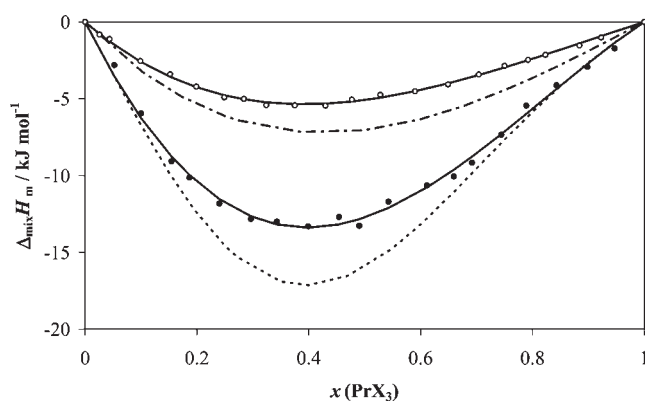
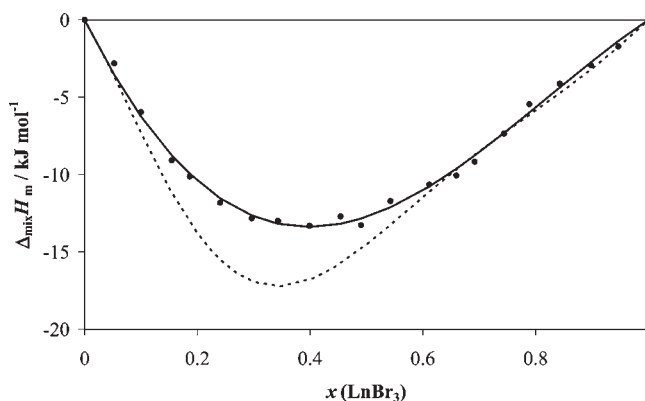
$\Delta_{\text{mix}}H_m$		$\lambda$		$\Delta_{\text{mix}}H_m$		$\lambda$	
$x(\text{PrBr}_3)$	$\text{kJ}\cdot\text{mol}^{-1}$	$\text{kJ}\cdot\text{mol}^{-1}$	$x(\text{PrBr}_3)$	$\text{kJ}\cdot\text{mol}^{-1}$	$\text{kJ}\cdot\text{mol}^{-1}$	$x(\text{PrBr}_3)$	$\text{kJ}\cdot\text{mol}^{-1}$
0.032	−2.379	−76.801	0.514	−15.628	−62.561		
0.054	−4.196	−82.139	0.554	−14.002	−56.660		
0.073	−5.691	−84.098	0.606	−13.158	−55.109		
0.101	−7.273	−80.101	0.653	−11.543	−50.942		
0.121	−9.314	−87.571	0.682	−10.746	−49.549		
0.152	−11.384	−88.319	0.725	−8.518	−42.723		
0.181	−13.147	−88.687	0.757	−7.765	−42.212		
0.200	−14.368	−89.803	0.791	−6.619	−40.038		
0.251	−15.783	−83.952	0.837	−4.775	−34.999		
0.301	−16.809	−79.891	0.875	−4.747	−43.401		
0.353	−17.118	−74.950	0.915	−2.660	−34.201		
0.404	−16.976	−70.503	0.956	−1.758	−41.793		
0.467	−16.031	−64.404					

**Table 4.** Molar Enthalpies of Mixing  $\Delta_{\text{mix}}H_m$  and Interaction Parameters  $\lambda$  of the  $\text{PrBr}_3$ – $\text{CsBr}$  Liquid System at  $T = 1070$  K

$\Delta_{\text{mix}}H_m$		$\lambda$		$\Delta_{\text{mix}}H_m$		$\lambda$	
$x(\text{PrBr}_3)$	$\text{kJ}\cdot\text{mol}^{-1}$	$\text{kJ}\cdot\text{mol}^{-1}$	$x(\text{PrBr}_3)$	$\text{kJ}\cdot\text{mol}^{-1}$	$\text{kJ}\cdot\text{mol}^{-1}$	$x(\text{PrBr}_3)$	$\text{kJ}\cdot\text{mol}^{-1}$
0.032	−2.828	−91.296	0.471	−18.369	−73.724		
0.051	−4.689	−96.882	0.526	−18.517	−74.268		
0.096	−8.712	−100.387	0.576	−16.582	−67.897		
0.151	−13.097	−102.161	0.650	−14.595	−64.153		
0.199	−15.888	−99.674	0.696	−13.480	−63.710		
0.241	−17.945	−98.103	0.758	−11.260	−61.384		
0.301	−18.942	−90.028	0.806	−9.558	−61.127		
0.357	−19.302	−84.085	0.849	−6.925	−54.017		
0.400	−18.835	−78.479	0.894	−5.424	−57.236		
0.434	−19.022	−77.437	0.948	−2.960	−60.054		

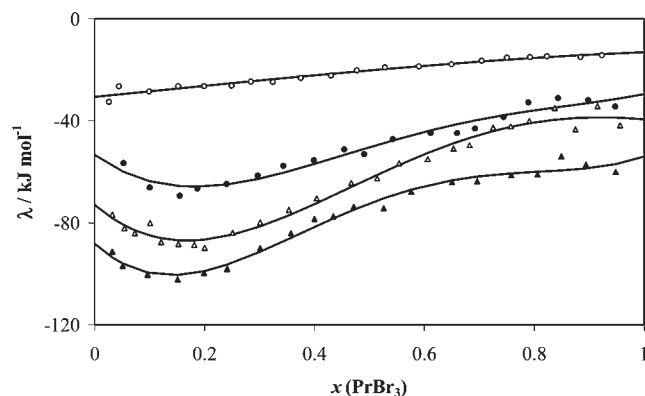
### 3. RESULTS AND DISCUSSION

The calorimetric experiments were performed at 1070 K over the entire composition range for the systems with NaBr, KBr,

**Figure 1.** Molar enthalpies of mixing  $\Delta_{\text{mix}}H_m$  of the  $\text{PrBr}_3$ – $\text{MBr}$  liquid systems:  $\circ$ , NaBr;  $\bullet$ , KBr;  $\triangle$ , RbBr;  $\blacktriangle$ , CsBr.**Figure 2.** Molar enthalpies of mixing  $\Delta_{\text{mix}}H_m$  of the  $\text{PrBr}_3$ – $\text{MBr}$  ( $M = \text{Na}, \text{K}$ ) and  $\text{PrCl}_3$ – $\text{MCl}$  ( $M = \text{Na}, \text{K}$ ) liquid systems:  $\circ$ ,  $\text{PrBr}_3$ – $\text{NaBr}$ ; dotted line,  $\text{PrCl}_3$ – $\text{NaCl}$ ;  $\bullet$ ,  $\text{PrBr}_3$ – $\text{KBr}$ ; dashed line,  $\text{PrCl}_3$ – $\text{KCl}$ .**Figure 3.** Molar enthalpies of mixing  $\Delta_{\text{mix}}H_m$  of the  $\text{PrBr}_3$ – $\text{KBr}$  ( $\bullet$ , solid line) and  $\text{TbBr}_3$ – $\text{KBr}$ <sup>15</sup> (dashed line) liquid systems.

RbBr, and CsBr. The results obtained are presented in Tables 1 to 4 and are plotted against composition in Figure 1. Three decimals (without physical meaning), in the presentation of thermodynamic values, are in accordance with the recommendation of the CODATA Task Group on Chemical Thermodynamic Tables.<sup>9</sup>

All of the melts are characterized by negative enthalpies of mixing with a minimum value of approximately (−5.4, −13.4,



**Figure 4.** Variation of the interaction parameter  $\lambda$  with composition for the  $\text{PrBr}_3$ -MBr liquid systems:  $\circ$ , NaBr;  $\bullet$ , KBr;  $\triangle$ , RbBr;  $\blacktriangle$ , CsBr.

**Table 5.** Least-Squares Coefficients for the  $\lambda$  Equation for Liquid Praseodymium(III) Bromide-Alkali Bromide Mixtures:  $\lambda$  ( $\text{kJ} \cdot \text{mol}^{-1}$ ) =  $A + Bx + Cx^2 + Dx^3 + Ex^4$  and Standard Deviation (SE, in  $\text{kJ} \cdot \text{mol}^{-1}$ )

system	A	B	C	D	E	SE
Pr-Na	-30.659	21.855	-2.298	-1.988		1.040
Pr-K	-53.386	-156.759	597.673	-672.154	255.050	2.354
Pr-Rb	-73.081	-182.913	713.030	-725.284	228.826	2.435
Pr-Cs	-88.247	-197.148	945.412	-1237.810	523.766	2.112

-17.1, and -19.3)  $\text{kJ} \cdot \text{mol}^{-1}$ , for M = Na, K, Rb, and Cs, respectively. Similarly, like in the case of  $\text{CeBr}_3$ -MBr liquid mixtures,<sup>7</sup> the minimum of the enthalpy of mixing is shifted toward the alkali bromide-rich compositions and is located in the vicinity of  $x(\text{PrBr}_3) \sim 0.4$ . The magnitude of the mixing enthalpy depends on the ionic radius of the alkali metal (Figure 1). The smaller the ionic radius, the smaller the absolute value of mixing enthalpy and the enthalpy minimum location shifted more toward the alkali bromide-rich compositions. Accordingly, the absolute value of the mixing enthalpy is the largest for the system with CsBr and decreases in the sequence from CsBr to NaBr (as does ionic radius of  $M^+$ ).

The mixing enthalpy also depends on the ionic radius of the common halide ion. As displayed in Figure 2, when this radius increases [from chloride to bromide, (181 and 196) pm, respectively<sup>10</sup>], a significant decrease of the mixing enthalpy is observed. For example, the minimum of the molar mixing enthalpy is of about  $-7.3 \text{ kJ} \cdot \text{mol}^{-1}$  and  $-17.1 \text{ kJ} \cdot \text{mol}^{-1}$  for the systems  $\text{PrCl}_3$ -NaCl and  $\text{PrCl}_3$ -KCl,<sup>11</sup> whereas in analogous  $\text{PrBr}_3$ -based bromide systems these values are ( $-5.4$  and  $-13.4$ )  $\text{kJ} \cdot \text{mol}^{-1}$ , respectively.

Finally, the mixing enthalpy in  $\text{LnX}_3$ -MX liquid systems is dependent on the ionic radius of lanthanide(III) cation. In Figure 3 the mixing enthalpy was plotted against molar fraction of the lanthanide halide for  $\text{PrBr}_3$ -KBr and  $\text{TbBr}_3$ -KBr.<sup>12</sup> The decrease of the  $\text{Ln}^{3+}$  ionic radius from 101.3 pm ( $\text{Pr}^{3+}$ ) to 92.3 pm ( $\text{Tb}^{3+}$ )<sup>10</sup> results both in an increase of the absolute value of the mixing enthalpy, when compared to analogous alkali metal systems, and shifting of the mixing enthalpy minimum toward alkali halide-rich compositions.

Figure 4 shows the composition dependence of the interaction parameter  $\lambda$

$$\lambda = \Delta_{\text{mix}}H_m / (x(\text{PrBr}_3) \cdot (1 - x(\text{PrBr}_3)))$$

which is representative of the energetic asymmetry in these melts. The values of  $\lambda$  for the liquid systems under investigation are also included in Tables 1 to 4. For each system, the values of  $\lambda$  were fitted by the method of least-squares to a polynomial of the form

$$\lambda = A + Bx + Cx^2 + Dx^3 + Ex^4$$

where  $x$  is the mole fraction of  $\text{PrBr}_3$ . The coefficients  $A$ ,  $B$ ,  $C$ ,  $D$ , and  $E$  as well as the standard deviation (SE) are collected in Table 5. Figure 4 shows the dependence of the enthalpy interaction parameter  $\lambda$  on the mole fraction of  $\text{PrBr}_3$ . All of the systems have negative interaction parameters  $\lambda$ , whose absolute values increase sharply with an increase of the ionic radius of the alkali metal cation. All systems show more negative values of the interaction parameter in the alkali bromide-rich than in the praseodymium bromide-rich range.

The composition dependence of the interaction parameter  $\lambda$  for  $\text{PrBr}_3$ -MBr systems is identical to the dependence observed for  $\text{CeBr}_3$ -MBr systems<sup>7</sup> and can be attributed to the formation of  $\text{PrBr}_6^{3-}$  complexes in the melts. The possibility of octahedral  $\text{LnX}_6^{3-}$  complex formation in  $\text{LnX}_3$ -MX liquid mixtures was confirmed by Raman structural studies.<sup>13</sup>

#### 4. SUMMARY

The molar mixing enthalpies in the liquid praseodymium(III) bromide-alkali metal bromide systems have been measured over the whole composition range. All of the melts are characterized by negative enthalpies of mixing. The minimum of the enthalpy of mixing is shifted toward the alkali bromide-rich compositions and located in the vicinity of  $x(\text{PrBr}_3) \sim 0.4$ . The magnitude of the mixing enthalpy depends on the ionic radius of the alkali metal (the bigger radius the more negative the mixing enthalpy), the radius of the common halide ion (a significant decrease of the mixing enthalpy with an increase of this radius) and the ionic radius of the lanthanide(III) cation (a decrease of the  $\text{Ln}^{3+}$  ionic radius results both in an increase of the absolute value of the mixing enthalpy, when compared to analogous alkali metal systems and a shifting of the mixing enthalpy minimum toward alkali halide-rich compositions).

The composition dependence of the interaction parameter  $\lambda$  for the  $\text{PrBr}_3$ -MBr systems is indicative of  $\text{PrBr}_6^{3-}$  octahedral complex formation.

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#### ■ REFERENCES

- (1) Ingier-Stocka, E.; Rycerz, L.; Berkani, M.; Gaune-Escard, M. Thermodynamic and transport properties of the  $\text{PrBr}_3$ -MBr Binary Systems (M = Li, Na). *J. Mol. Liq.* **2009**, *148*, 40–44.

(2) Rejek, J.; Rycerz, L.; Ingier-Stocka, E.; Gaune-Escard, M. Thermodynamic and Transport Properties of the  $\text{PrBr}_3$ – $\text{KBr}$  Binary System. *J. Chem. Eng. Data* **2010**, *55*, 1871–1875.

(3) Rycerz, L.; Ingier-Stocka, E.; Berkani, M.; Gaune-Escard, M. Thermodynamic and transport properties of the  $\text{PrBr}_3$ – $\text{RbBr}$  binary system. *J. Alloys Compd.* **2010**, *501*, 269–274.

(4) Rycerz, L.; Ingier-Stocka, E.; Berkani, M.; Gaune-Escard, M. Phase Diagram and Electrical Conductivity of the  $\text{PrBr}_3$ – $\text{CsBr}$  Binary System. *Z. Naturforsch.* **2010**, *65a*, 859–864.

(5) Rycerz, L.; Chojnacka, I.; Berkani, M.; Gaune-Escard, M. Thermodynamic Functions of  $\text{PrBr}_3$  and Congruently Melting  $\text{M}_3\text{PrBr}_6$  compounds ( $\text{M} = \text{K}, \text{Rb}, \text{Cs}$ ). *J. Chem. Eng. Data* **2011**, *56*, 1293–1298.

(6) Kapala, J.; Rutkowska, I.; Chojnacka, I.; Gaune-Escard, M. Modelling of the thermodynamic properties of the  $\text{ABr}$ – $\text{CeBr}_3$  ( $\text{A} = \text{Li}$ – $\text{Cs}$ ) systems. *CALPHAD: Comput. Coupling Phase Diagrams Thermochem.* **2010**, *34*, 15–19.

(7) Rycerz, L.; Gaune-Escard, M. Calorimetric investigation of the  $\text{CeBr}_3$ – $\text{MBr}$  liquid mixtures ( $\text{M} = \text{Na}, \text{K}, \text{Rb}, \text{Cs}$ ). *J. Chem. Eng. Data* **2009**, *54*, 2622–2625.

(8) Gaune-Escard, M. Thermochemical methods. In *Molten Salts: From Fundamentals to Applications*, NATO Science Series; Gaune-Escard, M., Ed.; Kluwer Academic Publishers: Norwell, MA, 2002; Vol. 52, p 375.

(9) CODATA Thermodynamic Tables, Selection for Some Compounds of Calcium and Related Mixtures: A Prototype Set of Tables; Garvin, D., Parker, V. B., White, H. J., Eds.; Hemisphere Publishing Corporation: Bristol, PA, 1987.

(10) Sharpe, A. G. *Inorganic Chemistry*; Longman: New York, 1986.

(11) Gaune-Escard, M.; Rycerz, L.; Szczepaniak, W.; Bogacz, A. Calorimetric investigation of  $\text{PrCl}_3$ – $\text{NaCl}$  and  $\text{PrCl}_3$ – $\text{KCl}$  liquid mixtures. *Thermochim. Acta* **1994**, *236*, 59–66.

(12) Rycerz, L.; Gaune-Escard, M. Mixing enthalpies of  $\text{TbBr}_3$ – $\text{MBr}$  liquid mixtures ( $\text{M} = \text{Li}, \text{Na}, \text{K}, \text{Rb}, \text{Cs}$ ). *Z. Naturforsch.* **2001**, *56a*, 859–864.

(13) Photiadis, G. M.; Borresen, B.; Papatheodorou, G. N. Vibrational modes and structures of lanthanide halide-alkali halide binary melts:  $\text{LnBr}_3$ – $\text{KBr}$  ( $\text{Ln} = \text{La}, \text{Nd}, \text{Gd}$ ) and  $\text{NdCl}_3$ – $\text{ACl}$  ( $\text{A} = \text{Li}, \text{Na}, \text{K}, \text{Cs}$ ). *J. Chem. Soc., Faraday Trans.* **1998**, *94* (17), 2605–2613.